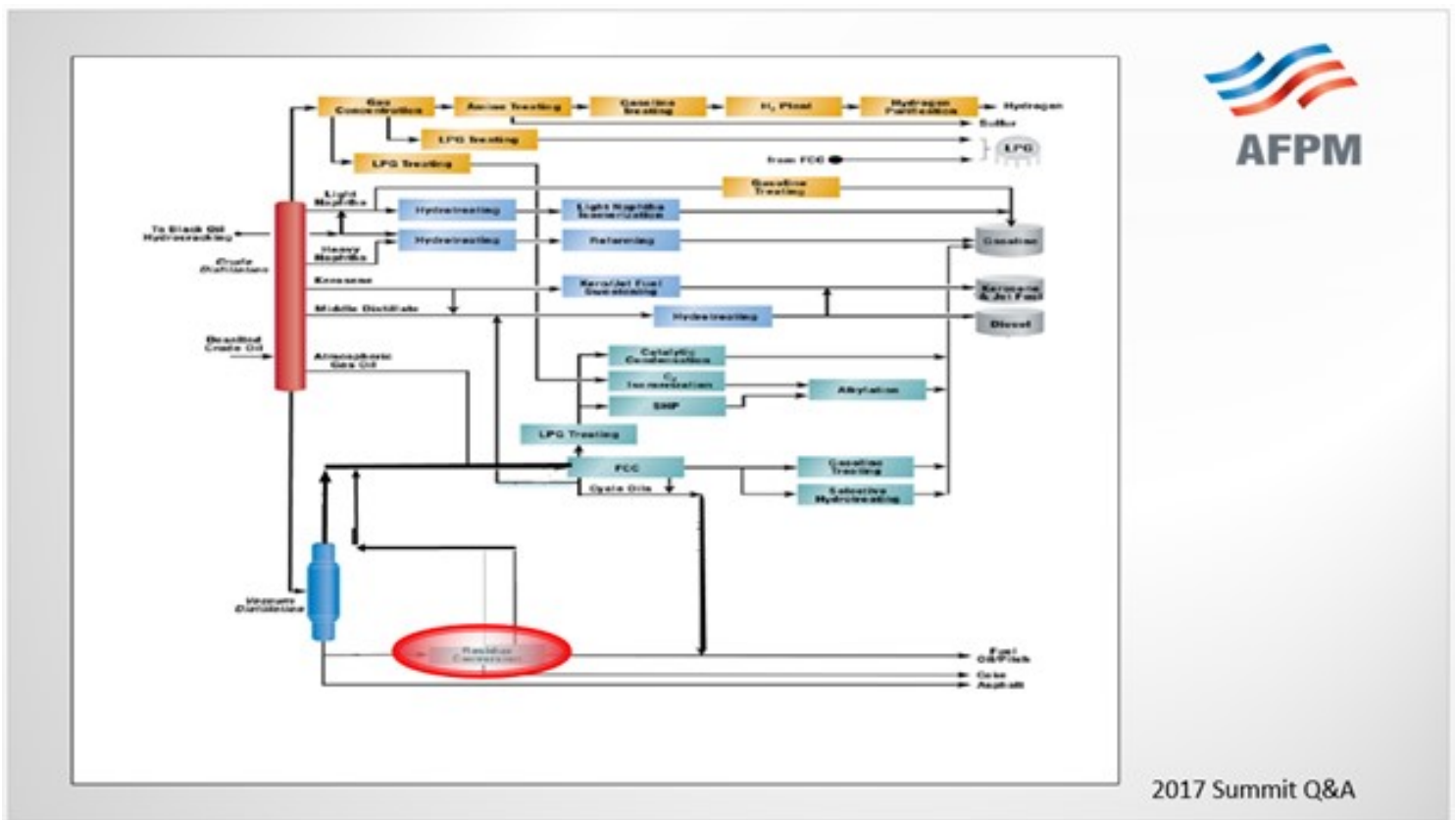


**Question 29: What is the impact of processing unconverted oil (UCO) from a high conversion hydrocracker on the following downstream units: FCC, coker, base-oil unit, and lubes hydrocracker?**

PAPPAL (Valero)

This question is a handful to cover in three minutes, but here we go. This is a generic refinery processing sour crude. First of all, we add a coker to this generic refinery.



2017 Summit Q&A

The heavy vacuum gasoil (HVGO) produced will be high in sulfur and nitrogen. The HVGO and the coker heavy gasoil (CHGO) are upgraded through the FCC. The CHGO, in this case, can be 14 gravities with 4,500 ppm of nitrogen. I want to acknowledge Jeff Bull, my colleague in San Antonio, who modelled these generic refinery configuration cases.



## What is the performance of the FCC in a base FCC/Coking refinery?

	<u>HVGO</u>	<u>CHGO</u>
<b>API</b>	15.8	14.0
<b>Sulfur, wt%</b>	3.5	4.3
<b>Nitrogen, ppmw.</b>	3500	4500
<b><u>Distillation, °F / °C</u></b>		
<b>10%</b>	770/410	647/342
<b>50%</b>	900/482	785/418
<b>90%</b>	1030/554	935/502

2017 Summit Hydroprocessing Q&A Session

In an FCC/coking refinery, running this HVGO/CHGO blend results in a very low FCC conversion level of about 63%. The FCC produces a great deal of cycle oil and slurry. In addition, the volume swell for this case is not very high.

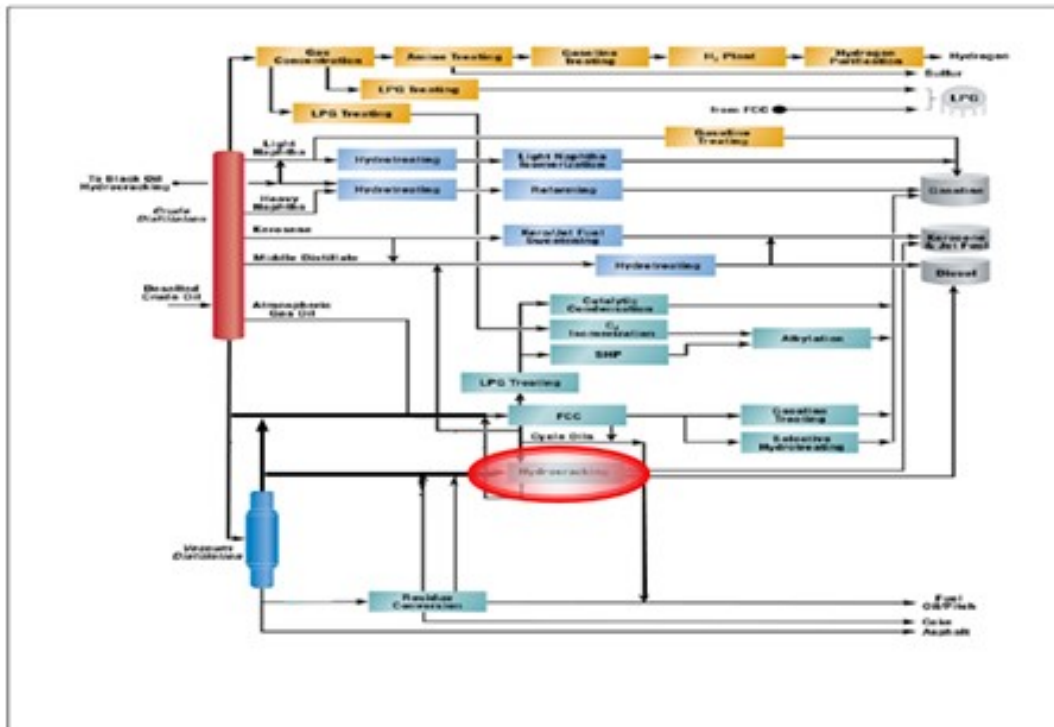


## FCC feed quality significantly impacts conversion activity

<u>FCC Yields (Volume Percent)</u>	<u>FCC/Coking Refinery</u>
Conversion	63.2
C3 + C4 Olefins	20.4
C5+ Naphtha	41.4
Light Cycle Oil	21.0
FCC Slurry	15.8
C3+ Total	105.2

2017 Summit Hydroprocessing Q&A Session

Now, we add a hydrocracker to this refinery configuration. Recall that we have the same crude slate, HVGO, and CHGO streams to upgrade. We add a reasonably powerful hydrocracker operating at 40 or 50% conversion.



2017 Summit Q&A

At this hydrocracker conversion level, many of the aromatics are converted and the sulfur and nitrogen are essentially completely removed. The unconverted oil from that hydrocracker operation is much improved at 35 gravity with virtually no sulfur or nitrogen, compared to the HVGO/CHGO feed to the hydrocracker. To stay in gasoil balance, the refinery would have to import HVGO or increase crude run. This scheme adds refinery G/D (gasoil/distillation) production ratio.



## What is the performance of the FCC in a base FCC/Coking/HCU refinery?

	<u>HVGO</u>	<u>UCO</u>
<b>API</b>	15.8	35
<b>Sulfur, wt%</b>	3.5	<.002
<b>Nitrogen, ppmw.</b>	3500	<5
<b><u>Distillation, °F / °C</u></b>		
<b>10%</b>	770/410	680/410
<b>50%</b>	900/482	900/482
<b>90%</b>	1030/554	1030/554

2017 Summit Hydroprocessing Q&A Session

The FCC operation in this configuration is much improved as the cat cracker conversion is over 80% instead of the low 60s without the hydrocracker. There is significant light olefin yield to produce alkylate and lots of gasoline for blending. FCC cycle oil yields are significantly lower, and C3+ volume swell increases by 10%. Likely, this is a more economic operation than the previous operation. The message here is that adding a partial conversion hydrocracker to a coking refinery can have a large impact on the operation and can improve the overall economics of this refinery.



## Hydrocracker UCO significantly improves FCC performance

<u>FCC Yields (Volume Percent)</u>	<u>FCC/Coking/HCU Refinery</u>
Conversion	80.4
C3 + C4 Olefins	26.5
C5+ Naphtha	56.2
Light Cycle Oil	14.1
FCC Slurry	5.5
C3+ Total	113.1

2017 Summit Hydroprocessing Q&A Session

To summarize, the FCC and coker operation can be decoupled as the hydrocracker converts aromatics. Potentially, the coker could produce a more difficult coker heavy gasoil; the hydrocracker would protect the FCC from that difficult feed. Our volumetrics in the coker and cat are decoupled a step further. If we were to add a deasphalter, our ability to run heavy crude would increase while staying within coking and FCC capacity limits. Adjustments to FCC and coking operation are likely needed. There is further opportunity to optimize crude.



## Impact of processing UCO from a high conversion hydrocracker on a Coker

- HCU allows coker and FCC performance to be decoupled
  - More difficult CHGO can be produced and upgraded through the HCU protecting FCC performance
  - Coker and FCC volumetrics can be decoupled
  - Addition of Deasphalter/HCU increases heavy crude run and premium product production.
  - Coker is unloaded

What is the impact of the hydrocracker on the lube block?







## Impact of processing UCO from a high conversion hydrocracker on a Base Oil Unit

- UCO as feed to a conventional base oil plant increases VI potential of product mix
- Base oil yield increases
- Unconventional lube crudes can be upgraded to produce premium lubricants

2017 Summit Hydroprocessing Q&A Session

If a catalytic lube configuration is producing Group 2 and Group 3 lubes, using the fuel's hydrocracker UCO as feed increases the high-quality base oil yield. The benefit is reduction of the lube hydrocracker conversion target required to meet the given VI target. Directionally, lube oil yield increases at lower tube hydrocracker conversion. Overall, the yield of premium quality base oil from that plant will increase.



## Impact of processing UCO from a high conversion hydrocracker on a Lubes Hydrocracker

- Processing UCO can increase high quality base oil product from existing HCU/HDW/HF complex
- Augments VI potential of the existing complex
  - Potentially lowers conversion target of lubes hydrocracker thereby increasing base oil yield

Print as PDF:

Tags

[Aromatics](#)

[Blending](#)

[Coker](#)

[Distillation](#)

---

Year

2017